# PHYSICS TODAY November 2023 • volume 76, number 11 A publication of the American Institute of Physics

URBULENT COLLECTO

Women astronomers at Yerkes

How bats tell food from clutter

New proxy for Earth's energy imbalance

The plume structure is visible in this numerical simulation of a sheared, thermally driven, turbulent Rayleigh–Bénard cell, viewed at a shallow angle above the cell's lower plate. Colors denote the variations in temperature. (Courtesy of Alexander Blass, University of Twente.) **Detlef Lohse** (d.lohse@utwente.nl) is the chair of the physics of fluids group at the University of Twente in Enschede, the Netherlands. **Olga Shishkina** (olga.shishkina@ds.mpg.de) is group leader at the Max Planck Institute for Dynamics and Self-Organization in Göttingen, Germany.



# Ultimate turbulent thermal convection

Detlef Lohse and Olga Shishkina

Recent studies of a model system—a fluid in a box heated from below and cooled from above—provide insights into the physics of turbulent thermal convection. But upscaling the system to extremely strong turbulence remains difficult.

> hermally driven turbulent flow can be found throughout nature and technology. Such flow transports not only heat but also mass and momentum. Comprehending what

determines that transport is key to understanding numerous geophysical and astrophysical flows and to being able to control the industrial and more general flows that people experience every day.

NOVEMBER 2023 | PHYSICS TODAY 27

## THERMAL CONVECTION



**FIGURE 1. THREE-DIMENSIONAL VISUALIZATION** of experimental turbulent structures (a) in half of a cylindrical Rayleigh–Bénard cell with diameter-to-height aspect ratio  $\Gamma = \frac{1}{2}$ , Rayleigh number  $Ra = 1.5 \times 10^9$ , and Prandtl number  $Pr \approx 0.7$  (see the main text for definitions). The particles with trails reveal small turbulent structures in the dominating large-scale convection, which has typical velocity U. The vertical component of the velocity,  $U_2$ , is plotted here, normalized by the so-called free-fall velocity  $U_f = \sqrt{\beta \Delta g L}$ . (Adapted from P. Godbersen et al., *Phys. Rev. Fluids* **6**, 110509, 2021.) (b) This cross-sectional snapshot from a fully resolved direct numerical simulation of a cylindrical convection cell with  $Ra = 10^{13}$ , Pr = 1, and  $\Gamma = \frac{1}{2}$  shows the dimensionless temperature field *T*, which varies from 0 at the top of the cell to 1 at the bottom. It reveals the tiny detaching plume structure. (Courtesy of Richard Stevens, University of Twente; based on an advanced finite-difference code developed by Roberto Verzicco, Tor Vergata University of Rome.)

Geophysical flows include the transport of heat in the atmosphere and the ocean, which determines weather, climate, ocean circulation, and the melting of ice shelves. Astrophysical examples include the transport of heat in the core and in the outer layer of stars and planets. Industrial examples include the transport of heat in chemical reactors and in electrolysis and other contexts of energy conversion. At the human scale, people most directly experience heat transport in the buildings, rooms, and vehicles whose temperature they control.

In all those systems, the fundamental question is, How much heat, mass, or momentum is transferred by the system? Direct measurements are difficult to make, as the geometries are often complicated, heat may leak out of the system, the boundary conditions may not be well known or well controlled, and global measurements may not be possible, given the length scales of the systems. What's more, direct numerical simulations may be prohibitive if the exact experimental boundary conditions are unknown.

Given those difficulties, the aim should be to understand real systems by using simple model systems, from which one can extrapolate the transport properties to the relevant flows. But developing those models requires a deep understanding of the system. That is especially true when the system undergoes a transition from one state to another—from a laminar-like state to a turbulent one, for instance—as then the transport properties of the flow can dramatically change. It is thus key to identify possible transitions between different states in such systems. The most famous and most frequently used model to study thermally driven flows is the Rayleigh–Bénard (RB) system. It consists of a flow in a closed box of height *L*, homogeneously heated from below through a hot bottom plate and cooled from above through a cold top plate. The flow is driven by the density differences between the lighter (usually hot) fluid, whose buoyancy makes it rise, and the heavier (usually cold) fluid, which sinks. Figure 1, which shows experimental and numerical snapshots of the flow field for strong thermal driving—to be quantified below—illustrates the complexity of the flow and the large-scale structure that evolves, which is known as the "wind of turbulence" (see the article by Leo Kadanoff, PHYSICS TODAY, August 2001, page 34).

RB convection has always been a popular playground in which to develop new concepts, such as instabilities, nonlinear dynamics, and the emergence of spatiotemporal chaos and patterns.<sup>1</sup> For very weak driving, the system has few degrees of freedom—it can be described using few coupled ordinary differential equations—but with increasing driving force it gains more degrees of freedom and eventually becomes turbulent.<sup>2.3</sup> The RB paradigm applies to heat transfer as well as mass transfer if it is driven by density differences—for example, in a system with heavier salty water at the top and lighter fresh water at the bottom, as can be found in the ocean and in industrial applications.

Several reasons account for the paradigm's popularity. The underlying dynamical equations—the Navier–Stokes equation, the advection–diffusion equation, and the continuity

# Rayleigh and Prandtl numbers

For a Rayleigh–Bénard (RB) cell of height *L*, with a temperature difference  $\Delta$  between the hot plate on the bottom and the cold plate on the top, the Rayleigh number *Ra* is defined as  $\beta g L^3 \Delta / (\nu \kappa)$ , where  $\beta$  is the thermal expansion coefficient, *g* the gravitational acceleration,  $\nu$  the kinematic viscosity, and  $\kappa$  the thermal diffusivity. The ratio  $\nu/\kappa$  is the Prandtl number *Pr*.

In principle, there are three methods for achieving large Rayleigh numbers in an RB system: Maintain a large  $\Delta$ , use a box with large *L*, and make sure *v* and  $\kappa$  are both small. But each method has its own caveats and difficulties.

Here are some typical values for the Rayleigh and Prandtl numbers: Convective fluid motion sets in at  $Ra \sim 2000$  for a large-enough aspect ratio of width to depth, independent of Pr. Under stronger forcing, the flow becomes turbulent, and much more complicated flow structures emerge, as shown in figure 1. For water, for which Pr typically ranges from 4 to 10, in a 20-cm-high container heated to 60 °C from below and cooled to 30 °C from above, Ra can reach up to  $10^{10}$ . In

equation—result from momentum, energy, and mass conservation, respectively. And the respective boundary conditions are well known, so the system is mathematically well defined. The RB system is closed, so that exact global balances between the forcing and the dissipation can be derived. It also has various symmetries, such as temporal and spatial translation symmetries, rotational symmetry, and, for small-enough temperature differences, top–bottom reflection symmetry; they make it attractive for theoretical approaches. And thanks to its simple geometry, the system is accessible to controlled experiments and to direct numerical simulations, provided the thermal driving is not too strong.

#### Dimensionless numbers

The most relevant question in turbulent RB convection is, How does the heat transport—that is, the time- and area-averaged vertical heat flux (in dimensionless form, the Nusselt number Nu, the ratio of convective to conductive heat transfer)—depend on the three dimensionless control parameters of the system? Those parameters are the Rayleigh number Ra (the nondimensionalized temperature difference  $\Delta$  between the hot and cold plates—that is, the thermal driving strength), the Prandtl number Pr (the ratio of the momentum diffusivity to thermal diffusivity), and the aspect ratio  $\Gamma$  (the ratio of the container's width to its height).

The box above lists some typical values for Ra and Pr in nature and technology. Both Nu and the Reynolds number Re (the ratio of inertial forces to viscous forces) are dependent on Ra, Pr, and  $\Gamma$ . Those dependencies are traditionally sought in the form of scaling laws:  $Nu \sim Ra^{\gamma}Pr^{\delta}$  and  $Re \sim Ra^{\xi}Pr^{\eta}$ . Researchers have tried to measure and understand those dependencies for at least the last 60 years.<sup>2,3</sup> And for the past 30 years, they have been helped by direct numerical simulations of the system.

#### Classical regime

In the regime of Rayleigh numbers up to  $Ra \sim 10^{11}$ —which has become feasible in many labs over the past three decades and is nowadays known as the classical regime of turbulent RB convection—researchers have reached broad agreement among various experiments and numerical simulations. Figure 2 shows Nu(Ra, Pr) for Prandtl numbers varying over six decades,  $10^{-3} \leq Pr \leq 10^3$ , in cylindrical cells with  $\frac{1}{2} \leq \Gamma \leq 1$ . Researchers have a good understanding of the regime, thanks to industrial applications with L = 20 m, the same temperature difference implies that Ra is roughly 10<sup>16</sup>.

In the atmosphere, where  $Pr \approx 0.7$ , values of Ra above  $10^{21}$  are not uncommon. In the ocean, assuming a water depth of 5 km, Ra can exceed  $10^{20}$ , whereas in the upper convective zone of the Sun or stars, it is on the order of  $10^{25}$ . Liquid metals, like those in Earth's core, typically have  $Pr \sim 0.01$ . The magma in Earth's mantle has  $Pr \sim 10^{20}$  because of the high viscosity, which typically leads to an Ra value of only  $10^6$  to  $10^7$ .

a unifying theoretical approach to wall-bounded turbulence developed by Siegfried Grossmann and one of us (Lohse).<sup>4</sup> Called the GL theory, it builds on the ideas of Ludwig Prandtl, Heinrich Blasius, Andrey Kolmogorov, and Sergei Obukhov.

The unifying theory uses two exact equations, which are straightforwardly obtained by volume integration and the divergence theorem from the Navier–Stokes equations for the velocity field  $\mathbf{u}(\mathbf{x}, t)$ , driven by the buoyancy force from the temperature, and from the advection equation for the temperature field  $\theta(\mathbf{x}, t)$ ; here  $\mathbf{x}$  denotes spatial coordinates and t, time. Assuming that the material properties apart from density are temperature independent, the two equations for the time- and volume-averaged viscous and thermal dissipation rates are, respectively,

$$\varepsilon_{u} \equiv v \langle (\partial_{i} u_{j}(\mathbf{x}, t))^{2} \rangle_{V} = \frac{v^{3}}{L^{4}} (Nu - 1) Ra Pr^{-2}, \text{ and}$$
$$\varepsilon_{\theta} \equiv \kappa \langle (\partial_{i} \theta(\mathbf{x}, t))^{2} \rangle_{V} = \kappa \frac{\Delta^{2}}{L^{2}} Nu.$$

Those equations are remarkable insofar as they connect volume-averaged quantities ( $\varepsilon_u$  and  $\varepsilon_{\theta}$ ) with the vertical heat transport, *Nu*. The basic assumption of the GL theory is that the physics inside the turbulent core—the bulk of the flow—is fundamentally different from that in the boundary layers (BLs), as shown in figures 3a–3b. Accordingly, the time- and volume-averaged viscous and thermal dissipation rates are composed of two parts, namely

$$\varepsilon_{u} = \varepsilon_{u,BL} + \varepsilon_{u,bulk} \quad (1)$$
  
and  
$$\varepsilon_{\theta} = \varepsilon_{\theta,BL} + \varepsilon_{\theta,bulk} \quad (2)$$

Because of the differing physics in the bulk and in the boundary layers, their scaling behaviors differ as well. That, in turn, rules out the traditionally assumed pure scaling behavior  $Nu \sim Ra^{\gamma}Pr^{\delta}$  and  $Re \sim Ra^{\xi}Pr^{\eta}$  over the full range of Ra and Pr.

How do the four individual contributions in equations 1 and 2 scale? In the turbulent bulk, the viscous and thermal dissipation rates  $\varepsilon_{u,bulk}$  and  $\varepsilon_{\partial,bulk}$  follow the 1941 Kolmogorov–Obukhov scaling relations for turbulent flow (Kolmogorov turbulence). In terms of the turbulent wind velocity *U* and the temperature difference  $\Delta$  between the plates, those relations



imply that  $\varepsilon_{u,\text{bulk}} \sim U^3/L$  and  $\varepsilon_{\theta,\text{bulk}} \sim \Delta^2 U/L$ . Those scaling relations cannot hold in the boundary layers near the walls, where viscosity and thermal diffusivity matter. There, as long as the driving is not too strong, the viscous and thermal dissipation rates  $\varepsilon_{u,\text{BL}}$  and  $\varepsilon_{\theta,\text{BL}}$  scale according to the Prandtl–Blasius theory for laminar-type boundary layers that develop along a solid horizontal plate when a fluid flow has relatively low velocity. (See the article by John D. Anderson Jr, Physics Today, December 2005, page 42.)

The splitting of wall-bounded turbulent flow into two regions in equations 1 and 2 can be understood by analogy to Prandtl's foundational insight from 1904 that the potential, or Bernoulli, flow around a plate cannot hold close to the plate itself but must be matched to boundary layers with quite different physics and scaling relations. Only with that insight could Prandtl have obtained the observed Reynolds-number dependence of the drag, as shown in figures 3d–3f. The GL theory follows the same spirit, but for wall-bounded turbulent flow, the outer flow is not of the Bernoulli type but of the Kolmogorov–Obukhov type.

The details of the GL theory are worked out in references 2 and 4. The theory describes the experimentally and numerically observed dependencies Nu(Ra, Pr) and Re(Ra, Pr) over six orders of magnitude in Ra and in Pr up to Ra of about  $10^{11}$ . The theory has proven its predictive power for Ra and Pr parameter ranges for which measurements were carried out only later. The team of Ke-Qing Xia (Chinese University of Hong Kong) measured for large Pr values, and the teams of Sven Eckert (Helmholtz Center Dresden-Rossendorf), Peter Frick (Polytechnical University of Perm), and Jonathan Aurnou (UCLA) measured for small ones.

The key idea of the GL theory—namely, to start from exact global balance equations and to split the dissipation rates into boundary-layer and bulk contributions—is quite general. It has also been applied successfully to various other turbulent flows, such as internally heated turbulence, double-diffusive convection—in which the flow velocity is coupled to both the temperature and the salinity—horizontal convection, and magnetohydrodynamically driven turbulence.

#### Experiments at large *Ra*

For very large thermal driving beyond  $Ra \sim 10^{11}$ , the experimental results for Nu(Ra, Pr) seem to contradict each other, as shown in figure 2: For very similar Pr, the Nu(Ra) dependencies are quite different in different experiments. For those large Ra, direct numerical simulations become increasingly difficult to

**FIGURE 2. HEAT TRANSPORT**, parameterized by the dimensionless Nusselt number *Nu* (the ratio of convective to conductive heat transfer), depends on the control parameters of the system—the Rayleigh number *Ra* and Prandtl number *Pr*. It is plotted here divided by  $Ra^{1/3}$ , so that differences can be better seen. Colors denote the Prandtl number dependence. The experimental and numerical data points, taken between 1997 and 2020, come from various groups, most of which are discussed and cited in this article. The solid lines were produced for various Prandtl numbers using the Grossmann–Lohse unified theory for Rayleigh–Bénard turbulence.<sup>4</sup>

perform because of the many degrees of freedom in the system; extremely fine computational grids are required to run the simulations. For many applications, including those in geological and astrophysical contexts, however, the large-*Ra* limit is of particular interest. So how can one extrapolate insights from the lab scale and numerical simulations at smaller *Ra* and estimate the heat transport and the turbulence intensity on geo- and astrophysical scales? And how can one perform experiments for very large values of *Ra* in order to scale up the RB system?

To open the large-*Ra* regime to experimental studies, the University of Chicago's Albert Libchaber and colleagues used helium gas close to its critical point in an RB system, as it has extremely low kinematic viscosity and thermal conductivity. In 1989 he and his coworkers<sup>5</sup> achieved *Ra* ~ 10<sup>14</sup>. Bernard Castaing, Philippe Roche, and coworkers in Grenoble, France, continued to pursue that line of research. In 1997, Castaing and his collaborators<sup>6</sup> found a transition around *Ra* ~ 10<sup>11</sup> toward a steeper effective scaling of roughly *Nu* ~ *Ra*<sup>0.38</sup>, much larger than has been seen at lower *Ra*, where the effective scaling exponent never exceeds  $\frac{1}{3}$ . They termed that new regime "ultimate."

In later work, Roche and his colleagues found the transition Rayleigh number to vary up to  $Ra \sim 10^{13}$ , depending mainly on the aspect ratio of the cell and the Prandtl number.<sup>7</sup> The transition was also evidenced by the buildup of fluctuations in the boundary layer at the same transition Rayleigh number, supporting the view that the transition is connected with a destabilization of the boundary layer—meaning that in the new regime, the flow in the bulk and in the boundary layers are both turbulent.

Russell Donnelly and coworkers at the University of Oregon followed Libchaber's path of using helium gas as the working fluid close to its critical point,<sup>8</sup> but they increased the height of the RB cell and achieved an even larger *Ra*, up to ~  $10^{15}$ . In those experiments, however, no transition to a regime with enhanced scaling dependence for *Nu* could be identified. Nor was there evidence for an enhanced scaling regime in team members' follow-up experiments, carried out by Joseph Niemela and Katepalli Sreenivasan<sup>9</sup> and by Ladislav Skrbek and coworkers.<sup>10</sup>

Guenter Ahlers and Eberhard Bodenschatz proposed another idea for how to achieve very large Ra—namely, to use pressurized sulfur hexafluoride as the working fluid. The advantage of using pressurized SF<sub>6</sub> in RB experiments is that over a very large Ra range the system keeps roughly the same Pr. Ahlers, Bodenschatz, and coworkers at the Max Planck Institute for Dynamics and Self-Organization in Göttingen, Germany, performed their experiments with SF<sub>6</sub> pressurized up to 19 bars, for which Pr remains roughly 0.7. In 2012 they observed a transition to an ultimate RB regime around  $Ra \sim 10^{14}$ 



**FIGURE 3. THE ANALOGY** between Rayleigh–Bénard flow and parallel flow along a flat plate. **(a–c)** In turbulent Rayleigh–Bénard convection, the core part of the flow is always turbulent (Kolmogorov turbulence), whereas the flow velocity along the wall drops to zero, as illustrated by the decreasing magnitude of blue arrows on each side in panel a. With increasing thermal driving strength—in other words, increasing Rayleigh number *Ra*—the boundary layers (BLs) change from a laminar (blue) Prandtl–Blasius type BL, with velocity profiles sketched in blue, to a turbulent (red) Prandtl–von Kármán type BL. The different cases have distinct dependencies of the heat transport (expressed by the Nusselt number *Nu*) on *Ra*, as shown, respectively, by the blue and red lines in panel c. **(d–f)** Parallel flow along a flat plate undergoes an analogous transition between laminar and turbulent BLs, each with different dependencies of the skin-friction coefficient *C<sub>f</sub>* on the Reynolds number *Re*, as sketched, respectively, with blue and red lines in panel f.

and with an aspect-ratio dependence consistent with the Grenoble results. The Nu dependence on Ra was steeper above the transition than below it and can be described with an effective scaling law  $Nu \sim Ra^{0.38}$  (see reference 11 and later papers by the Göttingen group). The sharp transition was found not only for Nu but also for Re and consistently at the same Ra. That observation also supports the view of a fundamental flow transition in an RB cell.

The discrepancy in the large-*Ra* regime between a typical Grenoble data set (with a transition toward an enhanced scaling around  $Ra \sim 10^{11}$ ), a typical Oregon data set (without a transition), and a typical Göttingen data set (with a transition around  $Ra \sim 10^{14}$ ) can be seen in figure 2. What is the origin of those different findings in the large-*Ra* experiments, even for very similar control parameters? At the moment, that's an open question.

# Ultimate turbulence regime

What do theories suggest about the existence of an ultimate regime? As early as 1962, Robert Kraichnan proposed an ulti-

mate regime of RB convection<sup>12</sup> and assumed a fully turbulent boundary layer and a certain scaling relation between Nu and Re for that boundary layer. He obtained  $Nu \sim Ra^{V_2}Pr^{V_2}$ , with logarithmic corrections. Note that in the ultimate regime, in no case can Nu grow faster than  $\sim Ra^{V_2}$ . That upper bound, which is much larger than any experimental or numerical data for Nu, was rigorously proved<sup>13</sup> by Louis N. Howard in 1963, with  $Nu - 1 \leq CRa^{V_2}$ , in which *C* is the constant  $\sqrt{3}/8$ . Other researchers verified the upper bound for slightly smaller values of *C* later.<sup>14</sup>

The GL theory of thermal convection<sup>4</sup> also suggests an ultimate regime: For large-enough driving strength, the laminar Prandtl–Blasius boundary layers, shown in figure 3a, should become unstable and undergo a transition toward turbulent boundary layers, the so-called Prandtl–von Kármán boundary layers (figure 3b). The transition is a direct analogue of the laminar-to-turbulent transitions of the boundary layers around a plate, as shown in figures 3d–3e or within a pipe. Those transitions are subcritical—meaning that around the transition different states coexist—and have a so-called nonnormal and nonlinear character, where nonnormal refers to the eigen-

## THERMAL CONVECTION

vectors of the linear operator being nonorthogonal. Such transitions have a double-threshold behavior: They can arise when the shear is sufficiently strong and disturbances (such as small wall roughnesses or thermal inhomogeneities in the plates) are large enough to trigger the onset.<sup>15</sup>

Typically, such an onset of shear instability in wall-parallel flow happens when the shear Reynolds number  $Re_s$  exceeds a value of about 420, as estimated by Walter Tollmien almost a century ago. The GL theory adopts Tollmien's value as a typical guideline for the onset of the shear instability (for  $\Gamma \sim 1$ ), although, of course, in the case of RB flow in a box, the flow is not strictly parallel to the wall. For  $Pr \approx 0.7$  and  $\Gamma \sim 1$ , the critical Rayleigh number for the onset of the ultimate regime in RB convection<sup>4</sup> can be estimated to be around  $10^{14}$ . But given the double-threshold feature of the transition, it may also be earlier or later for different small disturbances. For larger *Pr* or smaller  $\Gamma$ , the critical Rayleigh number increases.

What dependence Nu(Ra, Pr) should be expected in the ultimate regime? From an integration of the energy-dissipation rate in the turbulent boundary layer,<sup>16</sup> one obtains  $Nu \sim Ra^{\nu_2}Pr^{\nu_2}/(\log(Ra))^2$ , which in today's experimentally accessible regime implies an effective scaling of roughly  $Nu \sim Ra^{0.38}$ .

How then can one reconcile the various seemingly contradictory measurements of Nu(Ra, Pr) for  $Ra > 10^{11}$ , evident in figure 2? The analogy to pipe flow or other shear flows has been helpful to researchers, and over the past few years, they have made some intriguing suggestions as to why the Rayleigh numbers of the observed transitions to the ultimate regime depend on details of the different experiments. The key idea, proposed by Roche in 2020,<sup>7</sup> is to realize the subcritical nature of the transition, which has the above-mentioned double-threshold behavior and is the typical feature of transitions in shear flows,<sup>15</sup> applies in this case because of the strong local shear at the boundaries.

The subcritical nature of the transition implies that multiple states can coexist and that the transition is hysteretic—it depends on the system's history—and that for strong-enough shear, even quite small disturbances can trigger the transition from laminar flow to turbulent flow (notice the analogy between figure 3c and figure 3f). That interpretation has the potential to reconcile the various observations and different values of the Rayleigh number at which the transition occurs.

Although the transition toward an ultimate turbulence regime for RB turbulence is under intense discussion, no one disputes its relevance for Taylor–Couette (TC) turbulence.<sup>17</sup> The TC system—two coaxial corotating or counterrotating cylinders with fluid between them—is sometimes called the twin of the RB configuration because of many similarities between the two systems.<sup>18</sup> The analogy between RB and TC also holds in the ultimate regime and has been observed in all of the experiments and numerical simulations of turbulent TC flow made at large-enough driving strength.

That large-enough driving strength is more easily accessible in TC flow than in RB flow reflects the fact that the mechanical driving in TC flow is much more effective than the thermal driving in RB flow. Similarly, one should also expect an ultimate regime in pipe flow, horizontal convection, and other systems. Were the existence of an ultimate regime doubted in any of those flows, then one would have to come up with a mechanism by which the laminar flow in the boundary layers would remain laminar at arbitrarily large driving strength and the transition to turbulence would be suppressed. Frankly, we do not see what such a mechanism could be.

How then can the controversy on the ultimate regime in RB flow be settled? Given that striving toward ever-larger experiments and numerical simulations is extremely difficult and costly, one possibly promising route is to further explore the analogy to the laminar-to-turbulent transition in flow around a plate, illustrated in figure 3, or in pipe flow. In both cases a detailed analysis of the lifetime of disturbances of different strength has led researchers to conclude that the transition can be interpreted as a directed percolation transition.<sup>15</sup> Such a transition is quite universal in physics, and it also applies, for example, to epidemiological models for the spreading of diseases. One can hope that analogous experiments, as in pipe flow, and corresponding numerical simulations—including those in which Prandtl numbers vary—will further elucidate the fascinating transition to the ultimate regime.

The issue is of utmost relevance: Researchers must understand how to extrapolate the heat flux from controlled lab-scale experiments to the scales relevant in geophysical contexts. Whether a transition to an ultimate regime occurs or not will change the heat flux by orders of magnitude. But climate models and models for heat circulation in the ocean—with their implications for melting glaciers, nutrition transport, and the prediction of tipping points—clearly require more precision and reliability.

The scientific insights conveyed in this article come from more than three decades of collaborations and interactions with colleagues, postdocs, and doctoral students. We thank all of them for their contributions and for the intellectual pleasure we have enjoyed while working together. We thank Dennis van Gils for help with the figures.

#### REFERENCES

- 1. E. Bodenschatz, W. Pesch, G. Ahlers, Annu. Rev. Fluid Mech. 32, 709 (2000).
- 2. G. Ahlers, S. Grossmann, D. Lohse, Rev. Mod. Phys. 81, 503 (2009).
- D. Lohse, K.-Q. Xia, Annu. Rev. Fluid Mech. 42, 335 (2010); F. Chillà, J. Schumacher, Eur. Phys. J. E 35, 58 (2012); K.-Q. Xia, Theor. Appl. Mech. Lett. 3, 052001 (2013); O. Shishkina, Phys. Rev. Fluids 6, 090502 (2021).
- S. Grossmann, D. Lohse, J. Fluid Mech. 407, 27 (2000); S. Grossmann, D. Lohse, Phys. Rev. Lett. 86, 3316 (2001); R. J. A. M. Stevens et al., J. Fluid Mech. 730, 295 (2013).
- 5. B. Castaing et al., J. Fluid Mech. 204, 1 (1989).
- 6. X. Chavanne et al., Phys. Rev. Lett. 79, 3648 (1997).
- P.-E. Roche, New J. Phys. 22, 073056 (2020); P.-E. Roche et al., New J. Phys. 12, 085014 (2010).
- 8. J. J. Niemela et al., Nature 404, 837 (2000).
- 9. J. J. Niemela, K. R. Sreenivasan, J. Fluid Mech. 481, 355 (2003).
- 10. P. Urban et al., New J. Phys. 16, 053042 (2014).
- G. Ahlers et al., New J. Phys. 14, 103012 (2012); X. He et al., Phys. Rev. Lett. 108, 024502 (2012).
- 12. R. H. Kraichnan, Phys. Fluids 5, 1374 (1962).
- 13. L. N. Howard, J. Fluid Mech. 17, 405 (1963).
- F. H. Busse, *Rep. Prog. Phys.* **41**, 1929 (1978); C. R. Doering, P. Constantin, *Phys. Rev. E* **53**, 5957 (1996).
- P. Manneville, Mech. Eng. Rev. 3, 15 (2016); M. Avila, D. Barkley, B. Hof, Annu. Rev. Fluid Mech. 55, 575 (2023).
- 16. S. Grossmann, D. Lohse, Phys. Fluids 23, 045108 (2011).
- 17. S. Grossmann, D. Lohse, C. Sun, Annu. Rev. Fluid Mech. 48, 53 (2016).

PT

18. F. H. Busse, Physics 5, 4 (2012).